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Three-dimensionally ordered macroporous PrOx: an improved alternative to soot combustion ceria catalysts

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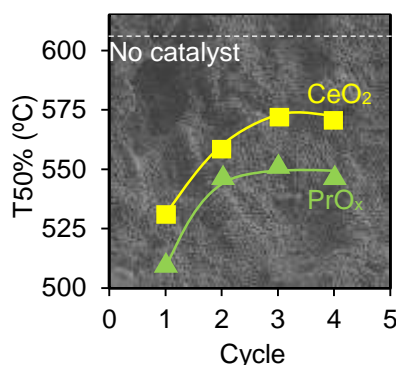
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Graphical abstract

Three-dimensionally ordered macroporous PrOx: an improved alternative to soot combustion ceria catalysts

ToC figure

**HIGHLIGHTS**

- A novel three dimensionally ordered macroporous (3DOM) PrO_x catalyst was prepared
- The soot combustion activity of 3DOM PrO_x was compared with 3DOM Ceria and conventional (Ref) catalyts
- 3DOM PrO_x is more active for soot combustion than 3DOM ceria
- PrO_x is more easily reducible than CeO₂ and 3DOM structure favors that reducibility
- PrO_x presents higher ability to oxidize NO to NO₂ than CeO₂ improving the activity

Abstract

The synthesis and use for soot combustion of praseodymium oxide with three-dimensionally ordered macroporous (3DOM) structure is described. This novel PrO_x-3DOM catalyst is presented as an improved novel metal-free alternative to CeO₂ as soot combustion catalyst. The PrO_x-3DOM catalyst presents a well-defined 3DOM structure with high macropores volume,

which significantly enhances the solid-solid soot-catalyst contact. This enhanced contact, together with the improved reducibility of PrO_x regarding CeO_2 , ameliorate the active oxygen production and its transfer to soot particles, improving the soot combustion with O_2 . In addition, the higher ability of PrO_x to oxidize NO to NO_2 , improves the soot combustion in a higher extent than CeO_2 in presence of NO_x . The catalytic activity of PrO_x -3DOM after several soot combustion cycles is also confirmed.

Keywords: soot, praseodymia, ceria, 3DOM, NO_x

1. INTRODUCTION

The main pollutants emitted by diesel engines are carbon particles and NO_x , together with certain amounts of CO and hydrocarbons [1,2]. These four compounds are responsible, in part, for the air pollution, and there is a set of requirements that regulate the permissible limits for the emissions of combustion gases from these vehicles [3,4]. In recent years, significant efforts

have been made in order to develop new systems to eliminate the carbon particles (soot) emitted by diesel engines, since these particles are responsible for severe environmental and health problems [5,6]. These systems usually consist of a filter placed in the exhaust pipe, where the particles are retained and burned [7–9]. Nevertheless, the temperature of the exhaust gases of modern diesel engines is relatively low (150–500 °C) [10,11] and consequently, is not enough for the spontaneous combustion of soot (550–700 °C) [12]. Thus, a catalyst is required to decrease the combustion temperature of retained particles.

Platinum-based catalysts are the best combustion catalysts in terms of activity and stability for a practical application [13–15]. However, the high cost and limited reserves of Pt are the main barrier for mass commercialization. Other alternative catalysts are being sought to try to improve or, at least, equalize the activity of these platinum catalysts but with lower cost. Cerium oxide is one of the most promising alternative catalysts, since ceria can generate highly reactive oxygen species, which are usually referred to as “active oxygen”. This active oxygen is highly oxidizing and very efficient for soot combustion [16–19]. Nevertheless, one of the main problems of this active oxygen-reaction pathway is the poor contact between the solid particles of carbon and the solid particles of catalyst. It has been demonstrated by several authors that the use of ceria with a three-dimensional ordered macroporous structure (3DOM) greatly improves the soot combustion due to the improvement of such solid-solid contact [20–24].

In addition to the active oxygen mechanism, ceria-catalyzed soot combustion could be also enhanced in presence of NO_x by the so-called “ NO_2 -assisted mechanism” [25]. However, only 5% of the NO_x present in the exhaust gases is NO_2 , and thus, NO has to be previously oxidized to NO_2 by the catalyst [25]. Ceria catalyzes the oxidation of NO to NO_2 in a certain extent, but the activity is much lower to that of platinum. However, opposite to platinum, NO_2 produced by a ceria catalyst can directly react with soot or can be adsorbed on ceria generating

more “active oxygen” by the decomposition of nitrogen-containing groups [26], both reaction pathways improving the soot combustion.

Praseodymium oxide could be presented as an improved alternative to ceria catalysts because of, akin ceria, can adopt oxygen-deficient stoichiometries, and even, the $\text{Pr}^{4+}/\text{Pr}^{3+}$ pair has a greater reduction potential than the $\text{Ce}^{4+}/\text{Ce}^{3+}$ pair, and moreover, presents higher ability for the NO_2 production [27]. Thus, both mechanisms described for ceria-catalyzed soot combustion could be enhanced in praseodimium catalysts. Herein we describe the synthesis of PrO_x -3DOM and its use, for the first time, in the soot combustion. Its behavior has been compared with that of CeO_2 -3DOM, and non-structured CeO_2 and PrO_x catalysts (which are referred to as “Ref” in this article) have been also prepared and tested for comparison.

2. MATERIALS AND METHODS

2.1. Catalysts preparation

PrO_x and CeO_2 catalysts have been prepared with conventional (Ref) and three dimensionally ordered macroporous (3DOM) structures. 3DOM catalysts were synthesized by infiltration of the metal precursor in a polymethylmethacrylate colloidal crystal template, which is then removed by calcination. Briefly, a polymethylmethacrylate (PMMA) colloidal crystals were prepared by polymerization of methylmethacrylate, methacrylic acid and divinylbenzene (100:1:5 volume ratio) in boiling aqueous solution. Polymerization was conducted for 75 min using potassium persulfate as polymerization initiator. After cooling, the colloidal crystals of PMMA were impregnated with an ethanolic precursor solution. This solution was prepared dissolving $\text{M}(\text{NO}_3)_3 \cdot 6\text{H}_2\text{O}$ (M: Pr or Ce) in ethanol (0.476 M) and adding citric acid in stoichiometric proportion to force the precipitation of metal citrates upon solvent evaporation. Afterwards, the solid was calcined at 600 °C for 6 hours with a heating rate of 1 °C/min to remove the PMMA template. The reference catalysts were prepared following the same

procedure but skipping the impregnation step, that is, the dissolution with citric acid and the M precursor was directly dried and calcined.

2.2. Catalysts characterization

SEM images were obtained in a Field Emission Scanning Electron Microscope (FESEM) Merlin VP Compact from Zeiss, working at very low voltages (from 0.02 kV to 30 kV) to minimize charging effects.

The porosity of catalysts was characterized by N₂ adsorption, mercury intrusion porosimetry and Helium density. N₂ adsorption-desorption isotherms were measured at -196 °C in an automatic volumetric system (Autosorb-6, Quantachrome) after degassing the catalysts at 150 °C for 2 hours under vacuum. The macroporosity of the catalysts was studied by mercury porosimetry in a Poremaster 60 GT (Quantachrome). The powdered catalysts were outgassed in this case at 50 °C under vacuum for 12 hours. The closed porosity was studied by helium pycnometry using an automatic helium pycnometer MicroUltrapyc 1200e (Quantachrome).

X-ray diffractograms were recorded in a Rigaku Miniflex II diffractometer, using CuK α radiation ($\lambda = 0.15418$ nm). Diffractograms were registered between 10 and 90° (2 θ) with a step of 0.025°. The average crystal sizes (D) were determined using the equation of Scherrer.

Temperature programmed reduction experiments were carried out with H₂ (H₂-TPR) in a thermobalance (Mettler Toledo; TGA/SDTA851) coupled to a mass spectrometer (Pfeiffer Vacuum; Thermostar GSD301T). The catalysts (20 mg) were heated in 5% H₂/Ar (40 ml/min) at 10 °C/min from room temperature until 900 °C.

XPS characterization was carried out in a K-ALPHA Thermo Scientific device, using Al-K α radiation (1486.6 eV). The X-ray spot was focussed on the catalysts with a diameter of

400 μm , at $3\text{ mA} \times 12\text{ kV}$. The binding energy scale was adjusted by setting the C1s transition at 284.6 eV.

2.3. Catalytic tests

Catalytic experiments at programmed temperature (25-700 $^{\circ}\text{C}$ at 10 $^{\circ}\text{C}/\text{min}$) were carried out in a fixed-bed tubular quartz reactor using a mixture of 20 mg of carbon black (Printex U), 80 mg of catalyst and 300 g SiC; prepared with a spatula in the so-called loose-contact mode in order to obtain results with practical meaning. Two gas mixtures were used (500 ml/min; GHSV = 30000 h^{-1}): 5% O_2/N_2 and 500 ppm NO/5% O_2/N_2 . The composition of the exhaust gases was controlled by a Specific NDIR-UV gas analyzers for CO, CO_2 , NO, NO_2 and O_2 (Fisher–Rosemount, models BINOS 100, 1001 and 1004).

3. RESULTS AND DISCUSSION

A polymethylmethacrylate colloidal crystal template (PMMA) was synthesized and impregnated with an ethanolic solution of praseodymium or cerium citrate prepared in situ by reaction of metal nitrate and citric acid. After template removal by air combustion, high-quality three-dimensional structures were obtained, consisting of an ordered network of macropores with a diameter of 80 nm approximately. This is observed in scanning electron microscopy images (**Figure 1a-b**). Well-defined 3DOM structures are observed for PrO_x -3DOM and CeO_2 -3DOM while Ref catalysts, obtained by direct calcination of the metal citrates, exhibit closed and compact structures (**Figure 1c-d**) with some evidences of gas release during the calcination step in the case of CeO_2 -Ref.

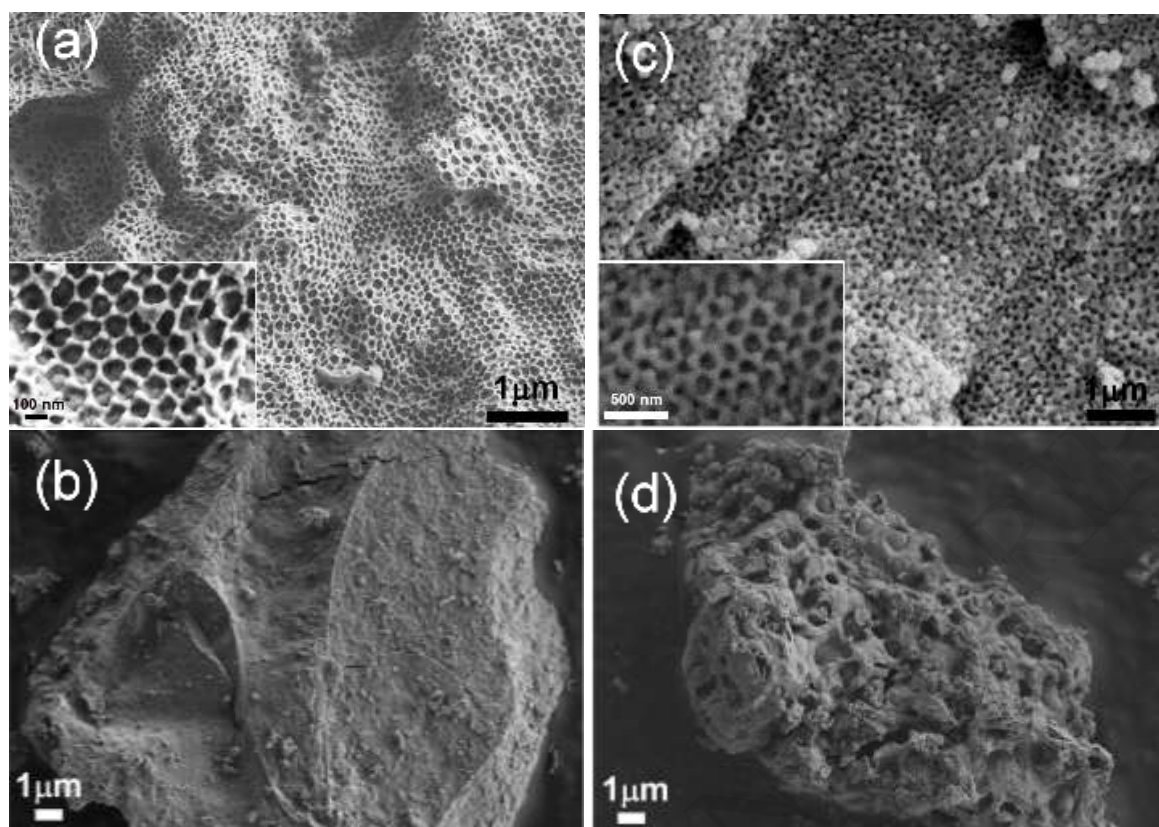


Figure 1. SEM images of a) $\text{PrO}_x\text{-3DOM}$, b) $\text{PrO}_x\text{-Ref}$, c) $\text{CeO}_2\text{-3DOM}$ and d) $\text{CeO}_2\text{-Ref}$.

This macroporous character of the 3DOM catalysts was confirmed by N_2 -adsorption and Hg porosimetry (**Figure 2**). Type II isotherms, characteristics of non-porous or macroporous adsorbent, were obtained for all catalysts. However, according with SEM images, significant differences are observed depending on the structure. 3DOM catalysts, as expected, present a strong and fast N_2 -adsorption at high relative pressures denoting the presence of high macropores volume. Both 3DOM catalysts show a well-defined peak in the pore-size distributions obtained by Hg porosimetry for pore radii around 40 nm (**Figure 2b**). $\text{PrO}_x\text{-3DOM}$ presents the highest macroporous volume because of the better-defined three-dimensional structure.

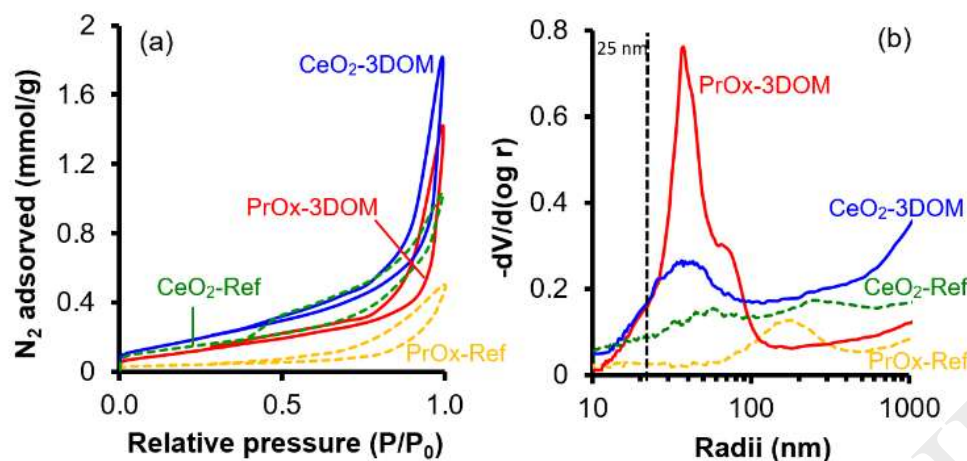


Figure 2. a) N₂-adsorption isotherms and b) Pore size distributions determined by mercury intrusion porosimetry.

Higher N₂-uptake is observed at low relative pressures in CeO₂-based catalysts regarding PrO_x ones, denoting the creation of certain microporosity during the gases release. The microporosity contribution to the apparent surface area (S_{BET}) is clearly observed in **Table 1**; higher surface areas were obtained for CeO₂ samples despite the lower macroporosity values.

Table 1. Results of catalysts characterization by N₂ adsorption, helium density, XRD and XPS.

[a] He density (ρ_{He}): expected He density values in brackets, [b] D: crystallite size, [c] V_{macro}: porosity volume up to 100 nm

Catalysts	S_{BET} (m ² g ⁻¹)	ρ_{He} [a] (cm ³ g ⁻¹)	D ^[b] (nm)	V _{macro} ^[c] (cm ³ g ⁻¹)	Carbonates ^[d] (%)	M ³⁺ [d] (%)	O _{ads} /O _{latt} ^[d]
CeO ₂ -Ref	13	6.9 (7.2)	21	0.108	12.1	34.4	0.23
CeO ₂ -3DOM	27	6.9 (7.2)	26	0.174	7.7	35.4	0.75
PrO _x -Ref	3	6.3 (6.9)	26	0.030	22.5	33.5	1.86
PrO _x -3DOM	10	6.6 (6.9)	26	0.265	20.3	52.6	2.01

obtained by Hg porosimetry, [d] data from XPS analysis (XPS spectra are included in the supplementary material file).

X-Ray diffractograms (included in the supplementary material file, **Figure S1**) reveal the stabilization of fluorite-structured cubic CeO_2 and Pr_6O_{11} , respectively, with fcc unit cells. Significant differences are not observed in d spacing and crystal sizes (**Table 1**), and consequently, crystallinity is not an important factor to take into account in the activity discussion.

Closed porosity was analyzed by He density measurements (**Table 1**). In all cases, the He density is lower than the expected value, denoting the existence of closed porosity, which is not accessible neither for He in density measurements nor for N_2 during adsorption-desorption. Note that this difference is more significant in PrO_x samples. This closed porosity is ascribed, in part, to the presence of carbonates [20–24]. The amount of carbonates determined by XPS is higher in the case of PrO_x samples (**Figure S2** and **Table 1**) and, either in CeO_2 and PrO_x catalysts, the carbonates amount decreases in 3DOM samples. These facts could be related to the basicity of the samples. It has been reported that both strength and number of basic sites are higher in Pr_6O_{11} regarding CeO_2 [28–30]. Since CeO_2 has lower basicity than Pr_6O_{11} , it alleviates the possibility of adsorption of CO_2 and the formation of carbonates. Moreover, it has been also reported that the basicity decreases increasing the M^{3+} concentration [31–33] and consequently, lower amount of carbonates is detected in 3DOM structures (see M^{3+} percentages in **Table 1**). A surface enrichment of M^{3+} ions is observed in 3DOM catalysts in comparison with Ref materials, denoting a surface oxygen deficiency in 3DOM materials. This fact is also corroborated by the higher $\text{O}_{\text{ads}}/\text{O}_{\text{latt}}$ ratio observed in 3DOM samples, since O_{ads} species are usually present at the oxygen vacancies and thus, a large amount of O_{ads} species implies a higher oxygen vacancy density. This higher surface oxygen vacancies in 3DOM samples could be ascribed to the O_2 -poor environment created during PMMA combustion. It is well accepted that the presence of oxygen vacancies is favorable for the improvement in reducibility.

Consequently, an improved reducibility could be expected in 3DOM samples and in PrO_x samples according with the $\text{O}_{\text{ads}}/\text{O}_{\text{latt}}$ ratio (**Figure S3** and **Table 1**).

The reducibility and the presence of carbonates/bicarbonates was studied by H_2 -TPR (**Figure 3**). The CO_2 desorption signal reveals the presence of different amount and strength of basic centres. A CO_2 peak at around 300 °C is obtained for PrO_x samples, whereas CeO_2 catalysts gave only a small desorption peak at around 120 °C, indicating lower and weaker basicity. In both cases, this peak decreases in 3D-structured samples according with previous observations. The reduction of the catalysts was followed by the m/z 18 signal. As expected, PrO_x catalysts are reduced at lower temperature and in a higher extent than CeO_2 ones, which is in agreement with the higher reduction potential of the $\text{Pr}^{4+}/\text{Pr}^{3+}$ pair. Bulk Pr^{4+} is reduced to Pr^{3+} between 400-600 °C, whereas bulk Ce^{4+} is reduced to Ce^{3+} at temperatures higher than 860 °C. Peaks at lower temperatures are observed for 3DOM samples. A peak at around 500 °C appears in CeO_2 , ascribed to surface ceria reduction, and around 250 °C in PrO_x samples.

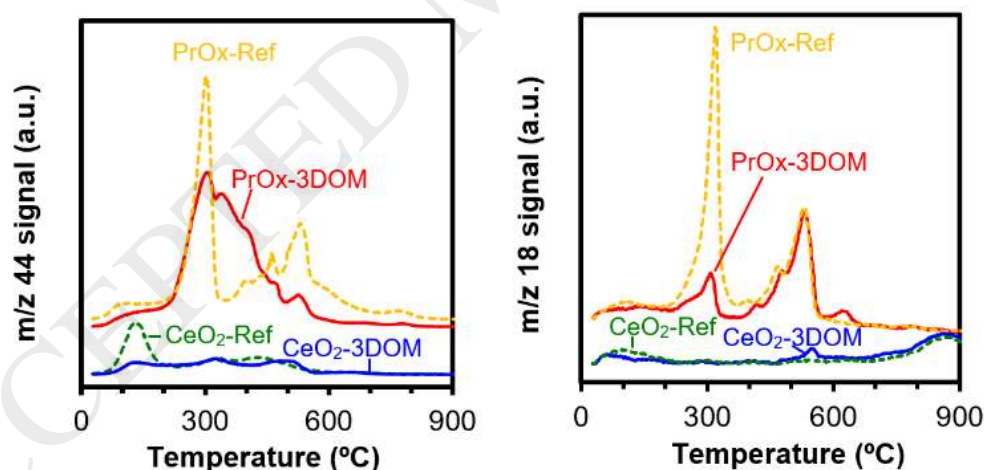


Figure 3. H_2 -TPR characterization of catalysts.

This improved reducibility is expected to improve the active oxygen generation and, consequently, the catalytic combustion of soot. This is confirmed in the catalytic experiments performed with O_2+N_2 (**Figure 4a**). In absence of NO_x , similar catalytic activities were obtained for Ref samples (**Figure 4a**) in spite of the different reducibility and oxygen vacancies

concentration of both inorganic oxides. Two factors must be considered in the “active oxygen” mechanism: the production of "active oxygen" (affected by the catalyst reducibility) and its transfer from the catalyst surface to the soot particles (affected by the soot-catalyst contact). The limited contact points between soot and catalyst in both Ref samples hinders the active oxygen transfer and, thus, similar activities are obtained in spite of the different active oxygen generation.

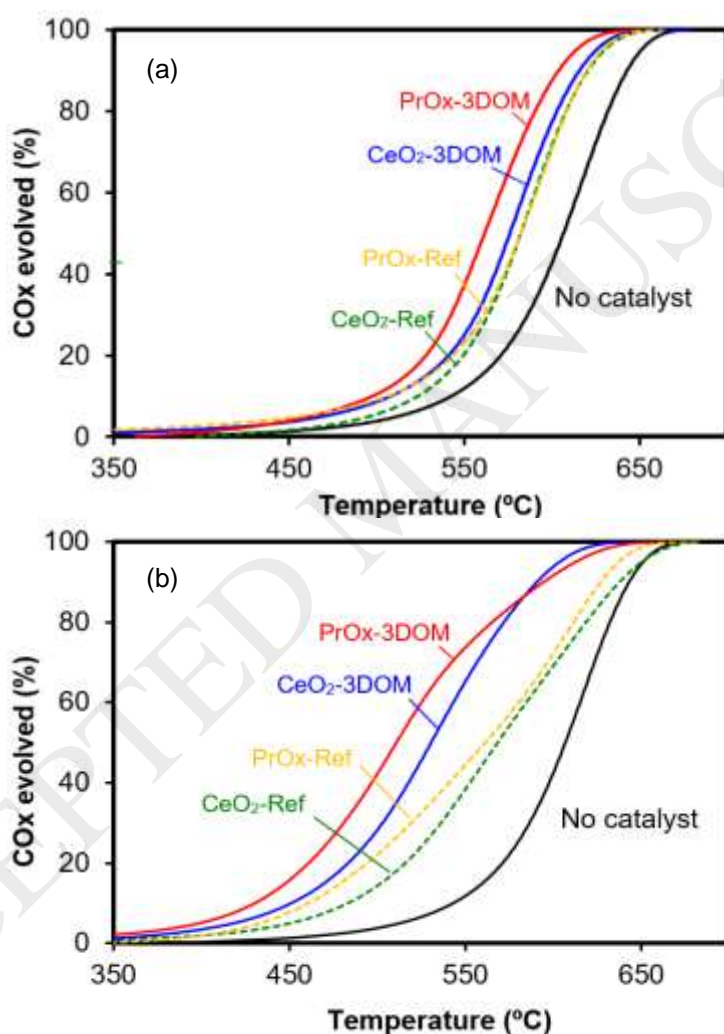


Figure 4. Soot combustion experiments with (a) 5% O₂ + N₂ and (b) 500 ppm NO_x + 5% O₂ + N₂.

The contact is improved by the development of 3DOM structures, improving the combustion activity. Nevertheless, the enhancement is more significant in the PrO_x -3DOM sample due to the better redox properties of this oxide.

A considerable activity enhancement is observed in presence of NO_x for all catalysts (see **Figures 4** and **5**). A significant decrease of the temperature for 50% soot combustion ($T_{50\%}$) is observed in presence of NO_x (**Figure 5**), and this decrease is higher in PrO_x catalysts, especially in the case of PrO_x -3DOM. The 3DOM structure also has an important role in this improvement.

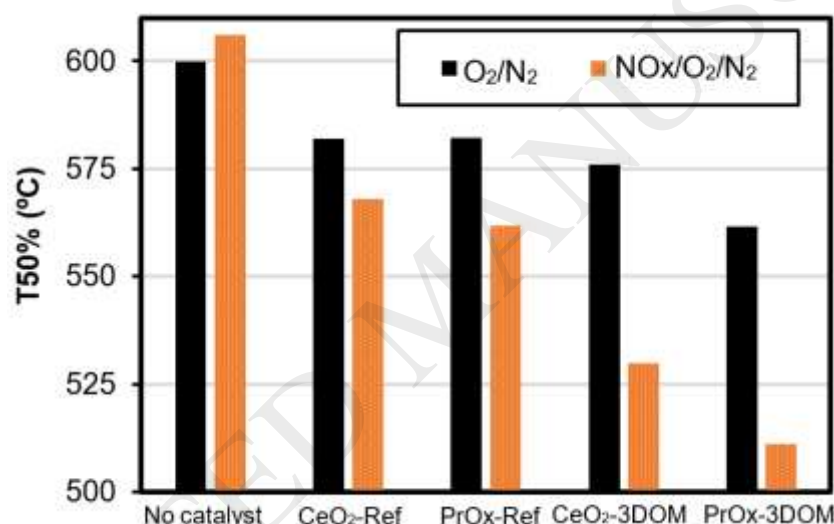


Figure 5. Comparison of soot combustion in the absence and presence of NO_x . ($T_{50\%}$ is the temperature where 50% of soot is oxidised in experiments shown in **Figure 4**).

Here, the ability of catalysts to oxidize NO to NO_2 (**Figure 6a**) has to be taken into account. The catalytic activity for NO oxidation to NO_2 is higher for PrO_x catalysts, and the 3DOM structure does not affect significantly this oxidation. NO_2 , once produced by the catalysts, reacts with soot, as confirmed comparing **Figures 6a** and **6b**, where the NO_2 profiles obtained in catalytic experiments without and with soot, respectively, are compiled. PrO_x

catalysts are more efficient in the combustion of soot in presence of NO_x due to their higher ability to oxidize NO to NO_2 .

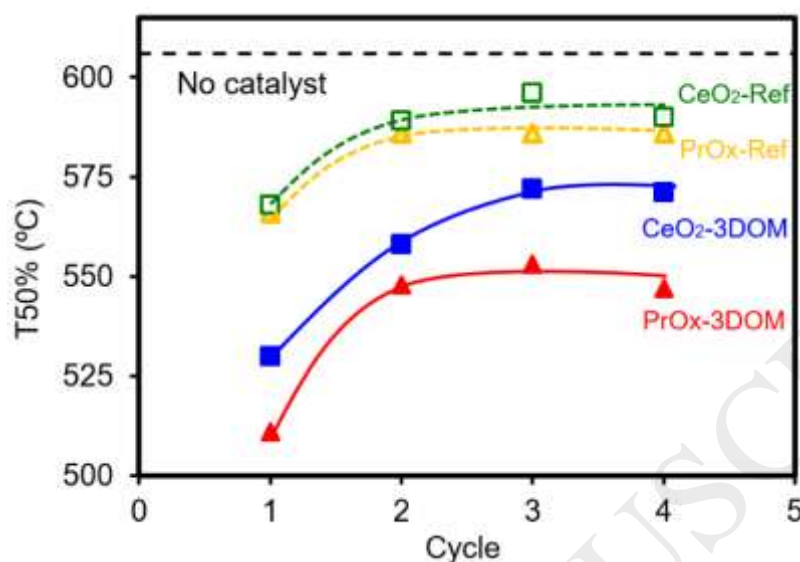


Figure 6. NO oxidation to NO_2 in catalytic experiments performed (a) without soot and (b) with soot.

Regarding the effect of the 3DOM structure in soot combustion with $\text{NO}_x + \text{O}_2 + \text{N}_2$, the explanation is more complex, since the structure does not affect NO_2 production. The 3DOM structure improves the soot-catalyst contact, and therefore, the active-oxygen mechanism is more efficient. NO_2 contributes to the creation of active oxygen, together with O_2 . NO_2 , once produced by the catalyst, can either travel in the gas phase and react directly with soot or can be re-adsorbed on the catalyst surface yielding NO and active oxygen [20]. Thus, NO_2 is an efficient way not only for direct soot oxidation but also for active oxygen production, and that is why the 3DOM structure is very positive for soot combustion also in the presence of NO_x , because NO_2 improves the active oxygen production and the 3DOM structure improves the transfer of active oxygen from catalyst to soot.

The catalysts deactivation after consecutive soot combustion cycles was also evaluated and results are collected in **Figure 7**. A loss of activity is observed in all catalysts after the first

combustion cycle, either for Ref and 3DOM catalysts. Nevertheless, once the activity is stable, PrO_x-3DOM keeps better activity than CeO₂-3DOM, and this is a promising result for the practical utilization of this novel material.

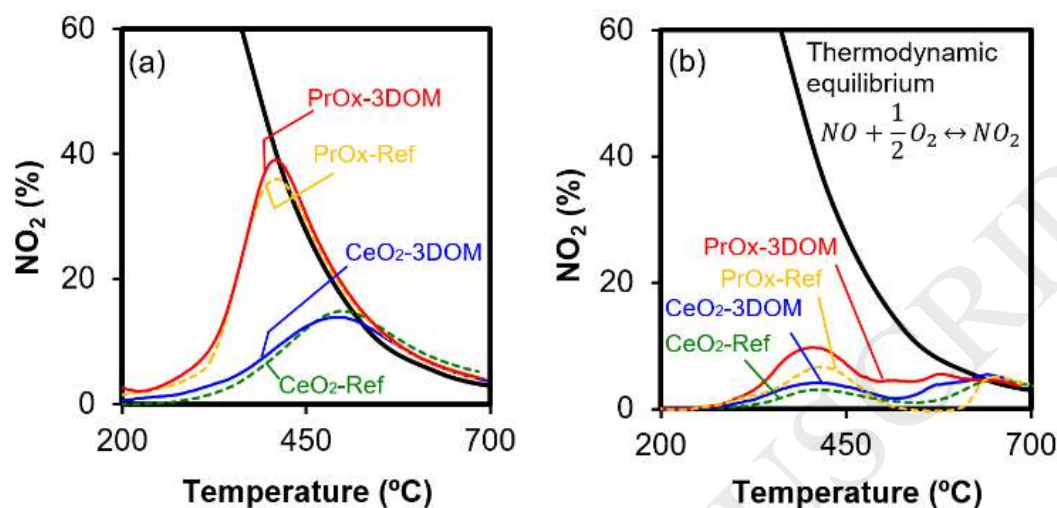


Figure 7. T50% for consecutive soot combustion cycles performed with 500 ppm NO_x + 5% O₂ + N₂.

The activity decrease of ceria catalysts during soot combustion experiments has been already reported, and two arguments can be appealed to explain this partial decrease. It is known that pure ceria sinters at high temperature [25], and this could partially explain the activity decrease observed in **Figure 7**. In addition, it is known that the catalytic oxidation of NO to NO₂ is an important step in the catalytic oxidation of soot. The catalytic oxidation of NO can involve both hydroxyls groups and surface oxygens on the ceria catalyst [34]. The participation of surface oxygen leads to the creation of oxygen vacancies that are filled in a further step by gas-phase molecular oxygen, while the participation of hydroxyl groups leads to the release of H₂O and also to the creation of oxygen vacancies. In this case, the population of hydroxyl groups cannot be restored under the experimental conditions of these experiments, and therefore, during consecutive soot combustion cycles, the surface chemistry of the catalysts is expected to change affecting the catalytic activity. These two arguments, sintering and change

of the surface chemistry, could explain the decrease of the catalytic activity observed in **Figure 7**.

4. CONCLUSIONS

In summary, it is reported the synthesis and use for soot combustion, for the first time, of three-dimensionally ordered macroporous PrO_x . From all the above results and discussion, the following conclusions can be drawn:

- i) A well-defined macroporous structure with a high volume of macropores has been obtained in the PrO_x -3DOM catalyst, which significantly enhances the catalyst-soot contact and thus, the activity.
- ii) PrO_x is more easily reducible than CeO_2 , and the 3DOM structure favors additionally that reducibility.
- iii) PrO_x presents higher ability to oxidize NO to NO_2 than CeO_2 , which participates in the generation of active oxygen favoring the soot combustion in higher extend.

Consequently, three-dimensionally ordered macroporous PrO_x presents an improved behaviour to generate active oxygen and to transfer it to soot, which provide an improved performance for the soot combustion with regard to ceria.

5. ASSOCIATED CONTENT

Supporting Information

6. ACKNOWLEDGEMENTS

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